Reaction Catalyzed by Montmorillonite: Polymerization of Methyl Methacrylate

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ABSTRACT: The polymerization of methyl methacrylate (MMA) was carried out in aqueous media having various concentrations of potassium persulfate as initiator in the presence or the absence of montmorillonite (Texas) at various temperatures. The rate of polymerization increased with increasing initiator concentration. Thermal stabilities of the resulting composite materials were studied and the activation energies of polymerization and degradation were determined. q 1997 John Wiley & Sons, Inc. J Appl Polym Sci **64:** 367–372, 1997

Key words: montmorillonite; methyl methacrylate; catalyst

treated natural clays were the preeminent solid catalysts used in petroluem refining, as they had the ability to induce vapor phase cracking of long **EXPERIMENTAL** chain molecules in crude oil to provide useful fuels for petrol engines. $2,3$

INTRODUCTION the presence of montmorillonite (Texas). The rate of polymerization using different concentrations Clays have been used for a variety of purposes of $(K_2S_2O_8)$ initiator with or without the catalyst
since prehistoric times. During this century, use has been determined. The activation energies of
has extended to the c

The organic chemist's interest in the use of MMA (BDH Chemicals, Ltd., U.K.) stabilized with $\frac{1}{N}$ was also kindled by the burst of activity 0.1% hydroquinone was washed with sodium hyclays was also kindled by the burst of activity $\frac{0.1\%}{2}$ hydroquinone was washed with sodium hy-
started in the 1970s when the potential of clay for droxide solution to remove inhibitor. The crude
solid acid catalysi solid acid catalysis and the utility of clay-sup-
norted reagents were described. Since that time a vacuum line, dried over anhydrous Na₂SO₄ and ported reagents were described. Since that time, a vacuum line, dried over anhydrous Na_2SO_4 and ported reagularize reagents of the catalytic stored below -18° C. Montmorillonite (English there have been numerous reports of the catalytic stored below -18° C. Montmorillonite (English activity of clay-based materials involving a tre-
china Clay Ltd.) and Al^{3+} -exchanged montmorilactivity of clay-based materials involving a tre-
mendous variety of organic reactions.^{4–6} hy standard ion-exchange intervals in the were prepared^{7,8} by standard ion-exchange The aim of this work is a study of the catalytic method using solutions of $Al(SO₄)_3$. 16H₂O. The ex-
lymerization of methyl methocrylate (MMA) in changed clay was repeatedly washed and centripolymerization of methyl methacrylate (MMA) in changed clay was repeatedly washed and centri-
fuged before drying in a vacuum oven at 60° C for 12 h. It was then ground and sieved at 140 mesh \circ 1997 John Wiley & Sons, Inc. CCC 0021-8995/97/020367-06 (ASTM). The material was then stored in a dry-

Catalyst (g)	Yield (g)	Yield $(\%)$		
0.00	1.485	31.6		
0.25	2.131	45.3		
0.50	3.091	65.8		
1.00	3.821	81.3		
1.50	3.880	82.6		
2.00	4.235	90.1		

Table I Effect of Weight of Catalyst in Polymerization of Methyl Methacrylate

air container. Potassium persulfate $(K_2S_2O_8)$ was a 55° C.
product of BDH Chemicals Ltd.

The reactions were carried out by dissolving the required amount of initiator in distilled water (45 mL) in a 250 mL conical flask into which MMA (4.7 g) was introduced. The montmorillon-
ite was added, and then the flask was well stop-
 $\frac{700\degree C}{700\degree C}$ under dynamic N. flow (60 mL/min) at a ite was added, and then the flask was well stop-
pered and put in a thermostated water bath for
the reaction time. The polymerization was
stopped by addition of hydroquinone (0.2 w/v % imes. The activation emperature to v and finally dried at 80° C for several days, the conversion was calculated from the relation

Conversion $(\%) = (Cp - C) \times 100/M$ **Hardness**

where Cp, C, and M are the weight of clay–poly-
mer composite, clay, and monomer, respectively. ball 2.5 nm and a load of 31.25 kg and 62.50 kg

made with a Mettler 3000TA thermobalance. The and sieved, and the powder having particle size

Figure 1 Effect of weight of catalyst on the yield of

Mechanical Properties

was used for the determination of the hardness of PMMA and MMA–clay polymer composite. The **Thermogravimetry (TG)** PMMA homopolymer and MMA–montmorillonite Thermogravimetry (TG) measurements were polymer composite materials (\sim 5 gm) were milled

Figure 2 Polymerization of MMA with 0.02 mol/L $K_2S_2O_8$: (a) MMA alone, (b) MMA with clay (106 μ m) at different temperatures.

Figure 3 Polymerization of MMA with 0.03 mol/L $K_2S_2O_8$: (a) MMA alone; (b) MMA with clay (106 μ m) at different temperatures.

õ200 mesh was molded by applying a pressure of **Effect of Initiator** 50 kg/cm^2 for 5 min at 180° C.

ferent weights of clay. Figure 1 indicates that the particle size of montmorillonite, due to the opencatalyst. Therefore, all the further experiments consequently to the increase of active centers.

Figures 2 through 5 show the conversion of MMA in the absence and in the presence of clay at vari-**Compression Strength Compression Strength ous temperatures by using 0.02, 0.03, 0.04, and** Compression strength measurements were made
with a Universal Testing Machine No. 15376, Lo-
sen-Housenwerk, of 40 tons capacity.
The percentage also increases by increasing the
the percentage also increases by increasing temperature and initiator concentrations. It seems that the catalytic effect of clay can be at-**RESULTS AND DISCUSSION** tributed to the formation of an addition product with potassium persulfate which must be active **Effect of Weight of Catalyst** enough to increase the rate of polymerization of methyl methacrylate. The activity of this addition Table I represents the conversion of MMA at dif-
product was found to increase with decreasing conversion reaches a limiting level using $1 g$ of ing of the framework of the montmorillonite and were carried out using 1 g of clay. Therefore, the catalytic effect of clay is attributed

Figure 4 Polymerization of MMA with 0.04 mol/L $K_2S_2O_8$: (a) MMA alone; (b) MMA with clay (106 μ m) at different temperatures.

Figure 5 Polymerization of MMA with 0.05 mol/L $K_2S_2O_8$: (a) MMA alone; (b) MMA with clay (106 μ m) at different temperatures.

to formation of an active complex with the initia-
a higher concentration of initiator, E_a decreases. tor, which increases the rate of polymerization more than for $K_2S_2O_8$ alone. This explanation was found to be in agreement with that suggested for
the polymerization of MMA in the presence of
soda lime glass,⁹ using sodium bisulfite as initia-
TG thermograms of PMMA and composi tor. It was found that the formation of an addition als of MMA–clay are shown in Figure 6. It is clear product between the glass powder and the initia- that the composite has higher stability than

tor increases the rate of polymerization of methyl methacrylate.

Activation Energy of Polymerization

Apparent activation energy, E_a , was determined from initial rate of polymerization of MMA with and without clay, at 55°, 60°, 65°, and 70°C. Plots of In K versus $1/T$ were made so that the activation energies could be determined by using the Arrhenius relationship. Table II shows that the activation energies of polymerization of MMA/*Ea* are higher in the absence of clay than in its presence, and at

TG thermograms of PMMA and composite materi-

Figure 6 TGA: (a) PMMA alone; (b) MMA–clay composite.

$K_2S_2O_8$ (mol/L)	PMMA			$MMA + Clay Composite$				
	0.02	0.03	0.04	0.05	0.02	0.03	0.04	0.05
Peak (1) T_{max} (°C)	273	280	284	286	278	287	288	290
Weight loss $(\%)$	25.9	21.05	20.70	18.50	15.02	15.5	18.8	19.1
Peak (2) T_{max} (°C)	360	365	368	370	365	368	371	378
Weight loss $(\%)$	62.3	61.8	60.9	60.2	50.1	47.32	39	36.89
Residue $(\%)$	11.8	17.1	18.8	21.45	34.85	39.29	35.5	40.52

Table III TGA of the PMMA and MMA–Clay Composite

centage weight losses for PMMA and MMA–clay composite. composite and the maximum rate of weight loss It seems that the increasing yield percentage shown by the derivative equipment associated increases the hardness and the compression with the TG apparatus. Strength of the materials. This indicates that

determine the rate of degradation from the initial the polymer composite. This is supported by the temperature of degradation. Measurements were part of polymer that was found to be insoluble carried out at 210, 220, 230, and 240° C, and the in benzene even when subjected to sohxlet exactivation energy of depolymerization was deter- traction for 24 h. mined using the Arrhenius equation. Table IV summarizes the results for some PMMA and MMA-clay composite. It is clear that the activation energy of degradation is in the same order **CONCLUSIONS** of polymerization and is in agreement with the thermal stability. The rate of polymerization of MMA, using potassium

Initiator $K_2S_2O_8$ $Concentration (mol/L)$

 cm^2 , respectively, while increasing to the ranges

Table IV Activation Energies of Degradation Table V Mechanical Properties of the PMMA With and Without Clay

PMMA homopolymer. Table III presents the per- of $30-38$ B.N. and $890-963$ kg/cm² in MMA clay

the polymer composites contain partly some polymer combined with montmorillonite. Therefore, increasing yield increases hardness and **Activation Energy of Degradation** compressive strength due to the higher combi-Isothermal kinetics were studied by using TG to nation between MMA and montmorillonite in

persulfate as initiator, increased in the presence of montmorillonite clay. The catalytic effect of clay in **Hardness and Compression Strength** the polymerization of methyl methacrylate is attrib-
the polymerization of methyl methacrylate is attrib-
ted to the formation of a clay/K₂S₂O₈ complex which Hardness and compression strength of PMMA
and MMA-clay were measured and are listed in
Table V. The hardness and compression strengths
of PMMA lie in the range $22-25$ B.N. and 620 kg/
particle by the polymer composite

- 1. A. R. Burridge, Ph.D. thesis, University of Wales 6. J. A. Ballantine, K. J. Davies, J. H. Purnell, M. (Swansea), 1991, 9. Ravanakorn, J. M. Thomas. and K. J. Williams, J.
- 2. T. H. Milliken, G. A. Miles, and A. D. Oblad, *Trans. Mol. Catal.,* **26,** 37 (1984).
- 3. K. Smith, *Solid Supports and Catalysts in Organic* (Swansea), 1992, 23. *Synthesis,* Ellis Horwood, U.K., 1992. 8. J. Williams, Ph.D. thesis, University of Wales
- 4. J. A. Ballantine, J. H. Purnell, M. Rayanakorn, (Swansea), 1988, pp. 27–29. J. M. Thomas, and K. J. Williams, *J.C.S. Chem.* 9. A. B. Moustafa and M. A. Diab, *J. Appl. Polym. Comm.,* **1,** 9 (1981). *Sci.,* **19,** 1585 (1975).
- **REFERENCES** 5. J. A. Ballantine, K. J. Davies, J. H. Purnell, M. Rayanakorn, J. M. Thomas, and K. J. Williams, *J.C.S. Chem. Comm.,* **9,** 427 (1981).
	- Rayanakorn, J. M. Thomas, and K. J. Williams, *J.*
	- 7. M. M. Al-Esaimi, Ph.D. thesis, University of Wales
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